

مقدمه  
روش‌های مورد استفاده



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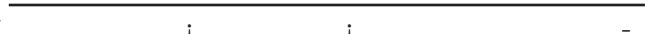
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چکیده

هدف از این مطالعه، تعیین میزان فلز آهن و هیدروژن پراکسید در منابع آب و خاک است. برای این منظور از روش‌های آنالیز گرافیکی و اسپکترومتری استفاده شد. نتایج نشان داد که روش‌های پیشنهادی حساسیت بالا، دقت خوب و بازه وسیع سنجش دارد. همچنین، این روش‌ها می‌تواند برای تعیین همزمان این دو پارامتر در نمونه‌های پیچیده استفاده شود. برای این منظور، از روش اسپکترومتری فلورسانس و آنالیز گرافیکی استفاده شد. نتایج حاصل از آنالیز نشان داد که این روش‌ها دارای دقت و حساسیت مناسبی است و می‌تواند به عنوان یک روش ساده و سریع برای تعیین این پارامترها در منابع آب و خاک استفاده شود. همچنین، برای تعیین همزمان این دو پارامتر، از روش اسپکترومتری استفاده شد. نتایج نشان داد که این روش‌ها دارای دقت و حساسیت مناسبی است و می‌تواند به عنوان یک روش ساده و سریع برای تعیین این پارامترها در منابع آب و خاک استفاده شود.

$(Fe^{2+} = \text{mmol/L})$   $Fe^{2+}/H_2O_2 = \text{mmol/L}$   $pH =$   $\text{mmol/L}$   $h$

واژگان کلیدی:



یافته‌ها و نتیجه‌گیری

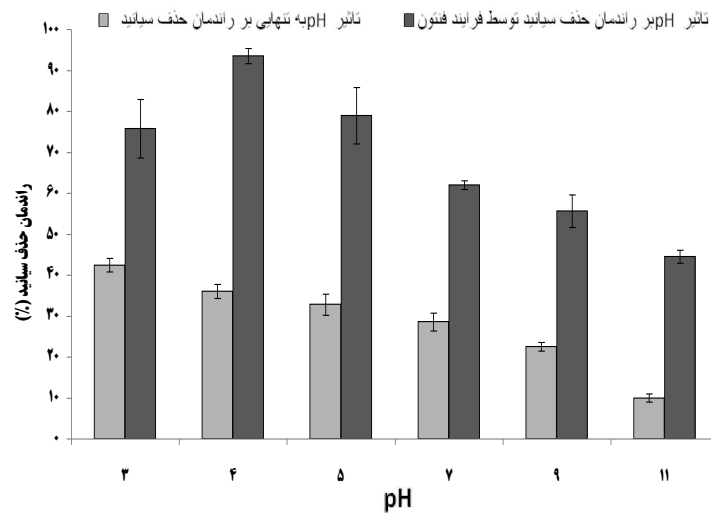
فصلنامه علمی پژوهشی انجمن علمی بهداشت محیط ایران، شماره چهارم، زمستان ۱۳۹۱

$$Fe^{2+} = \frac{y}{mmol/L} \quad Fe^{2+}/H_2O_2 = \frac{y}{y}$$

$$pH = \frac{fl}{L} , \quad fl \quad fl \quad L$$

$$\frac{fl}{L} - \frac{fl}{L} \quad fl \quad fl$$

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تأثیر pH نهایی بر راندمان حذف سیانید (mmol/L)  $Fe^{2+} = \bar{y}$  /  $H_2O_2 = \bar{y}$  /  $\bar{y}_{min}$  /  $\bar{y}$  mmol

تأثیر pH نهایی بر راندمان حذف سیانید (mmol/L)  $Fe^{2+} = \bar{y}$  /  $H_2O_2 = \bar{y}$  /  $\bar{y}_{min}$  /  $\bar{y}$  mmol

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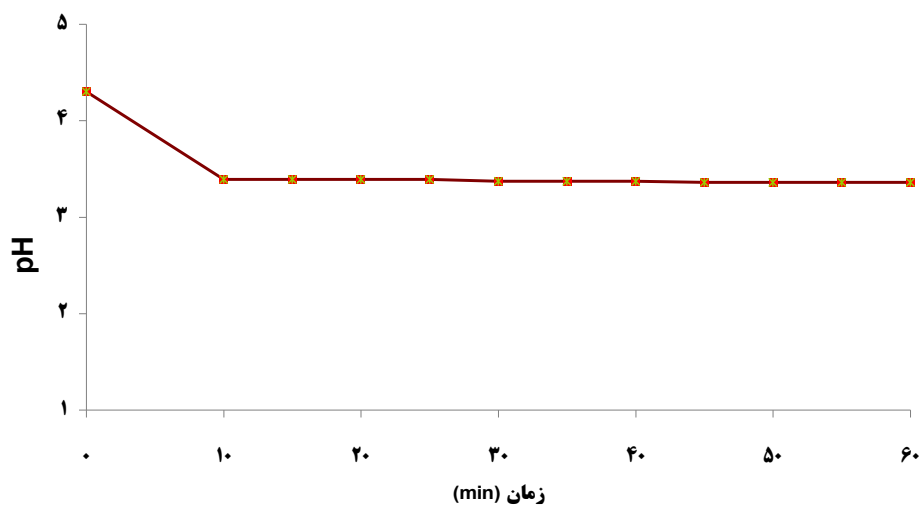
تأثیر pH نهایی بر راندمان حذف سیانید (mmol/L)  $Fe^{2+} = \bar{y}$  /  $H_2O_2 = \bar{y}$  /  $\bar{y}_{min}$  /  $\bar{y}$  mmol

تأثیر pH نهایی بر راندمان حذف سیانید (mmol/L)  $Fe^{2+} = \bar{y}$  /  $H_2O_2 = \bar{y}$  /  $\bar{y}_{min}$  /  $\bar{y}$  mmol

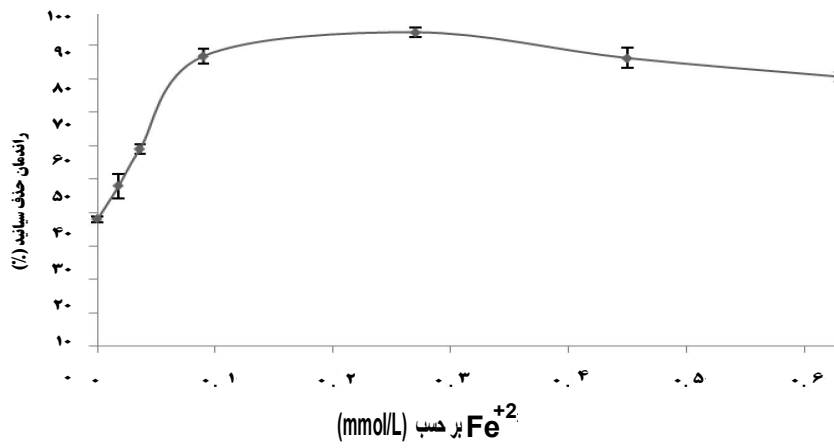
تأثیر pH نهایی بر راندمان حذف سیانید (mmol/L)  $Fe^{2+} = \bar{y}$  /  $H_2O_2 = \bar{y}$  /  $\bar{y}_{min}$  /  $\bar{y}$  mmol

تأثیر pH نهایی بر راندمان حذف سیانید (mmol/L)  $Fe^{2+} = \bar{y}$  /  $H_2O_2 = \bar{y}$  /  $\bar{y}_{min}$  /  $\bar{y}$  mmol

تأثیر pH نهایی بر راندمان حذف سیانید (mmol/L)  $Fe^{2+} = \bar{y}$  /  $H_2O_2 = \bar{y}$  /  $\bar{y}_{min}$  /  $\bar{y}$  mmol

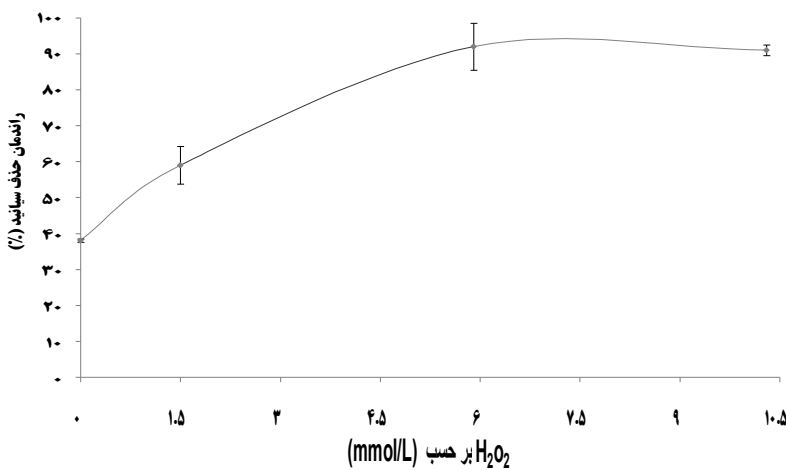


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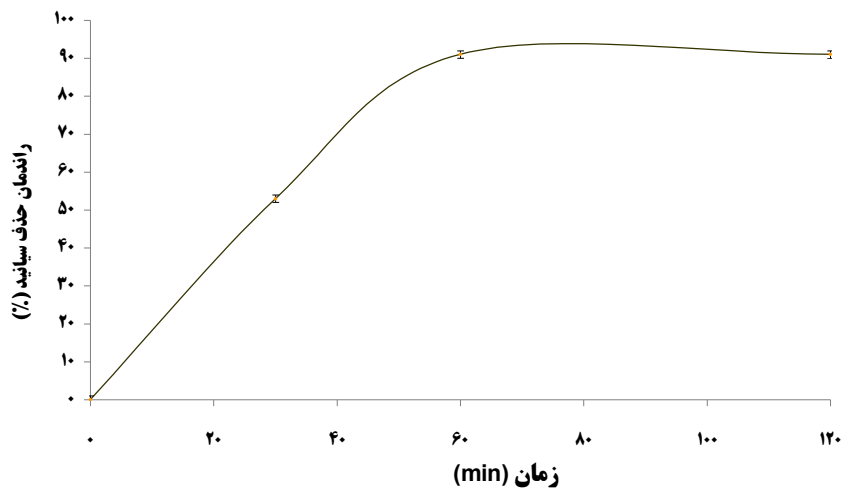


(Figure 1) Adsorption percentage of Fe<sup>2+</sup> vs. Fe<sup>2+</sup> concentration (mmol/L). Conditions: H<sub>2</sub>O<sub>2</sub> = 10 mmol/L, pH = 5, 30 min, 100 mg/L.

The adsorption percentage of Fe<sup>2+</sup> increases with increasing Fe<sup>2+</sup> concentration up to 0.3 mmol/L, after which it slightly decreases. This indicates that the adsorption capacity of the adsorbent is limited. The adsorption percentage of Fe<sup>2+</sup> is also affected by the concentration of H<sub>2</sub>O<sub>2</sub>, pH, and time. The adsorption percentage of Fe<sup>2+</sup> increases with increasing H<sub>2</sub>O<sub>2</sub> concentration up to 6 mmol/L, after which it slightly decreases. The adsorption percentage of Fe<sup>2+</sup> also increases with increasing pH and time.



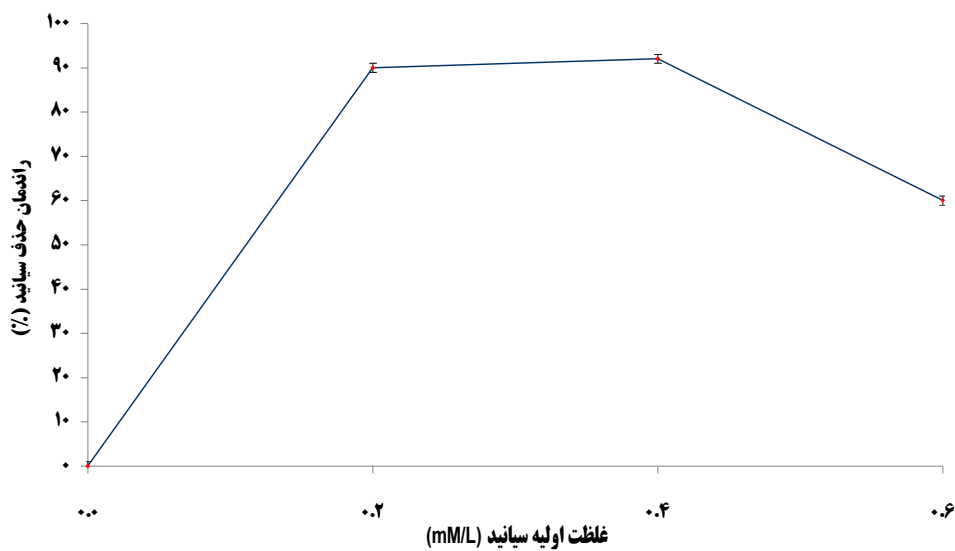
(Figure 2) Adsorption percentage of H<sub>2</sub>O<sub>2</sub> vs. H<sub>2</sub>O<sub>2</sub> concentration (mmol/L). Conditions: Fe<sup>2+</sup> = 10 mM/L, pH = 5, 30 min, 100 mg/L.



( $\text{Fe}^{2+} = \dots$  mmol/L)  $\text{Fe}^{2+}/\text{H}_2\text{O}_2 = \dots$  pH =  $\dots$  mmol

( $\text{Fe}^{2+} = \dots$  mmol/L)  $\text{Fe}^{2+}/\text{H}_2\text{O}_2 = \dots$  pH =  $\dots$  mmol

pH =  $\dots$  (Strong Acid dissociable  
 $\text{H}^+$  ) (H<sup>+</sup> ) pH =  $\dots$   
 / pH =  $\dots$  pH =  $\dots$



(mmol/L)  $\text{Fe}^{2+}/\text{H}_2\text{O}_2 = \dots$  i min pH =  $\dots$

( $\text{Fe}^{2+} = \dots$  mmol/L)  $\text{Fe}^{2+}/\text{H}_2\text{O}_2 = \dots$  i min pH =  $\dots$

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$\text{Fe}^{2+} / \text{H}_2\text{O}_2 < \text{pH} = \dots$   
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 ( fl )  
 Kavitha " ...  
 y mmol ...  
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 ( L y<sub>min</sub> ...  
 " H<sub>2</sub>O<sub>2</sub> ...  
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 mmol/L (H<sub>2</sub>O<sub>2</sub>:CN) = ...  
 è mg/L q<sub>min</sub> (Fe<sup>2+</sup>L y  
 Masahafi " ...  
 (H<sub>2</sub>O<sub>2</sub>:CN) = ...  
 mg/L èq<sub>min</sub> : éç mg/L  
 (é L ...  
 = y mmol/L ipH= q mmol/L  
 fFe<sup>2+</sup> / H<sub>2</sub>O<sub>2</sub> = y/y ) H<sub>2</sub>O<sub>2</sub> = / mmol/L iFe<sup>2+</sup>  
 n q<sub>min</sub> ...  
 " ...  
 q mmol ...  
 n q d q

$\text{Fe}^{2+} / \text{H}_2\text{O}_2 = \dots$   
 pH = L pH  
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 ( L  
 Fe<sup>2+</sup> pH  
 OH<sup>0</sup> H<sup>+</sup> H<sub>2</sub>O<sub>2</sub>  
 fl L OH<sup>0</sup>  
 Fe<sup>2+</sup> / H<sub>2</sub>O<sub>2</sub> = y/y  
 H<sub>2</sub>O<sub>2</sub> Fe<sup>2+</sup> "  
 ( L  
 $\text{Fe}^{2+} + \text{H}_2\text{O}_2 \rightarrow \text{Fe}^{3+} + \text{OH}^0 + \text{OH}^-$  ( )  
 Ly/y Fe<sup>2+</sup> / H<sub>2</sub>O<sub>2</sub> "  
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 $\text{Fe}^{2+} + \text{OH}^0 \rightarrow \text{Fe}^{3+} + \text{OH}^-$  ( )  
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 " y mmol  
 Fe<sup>2+</sup> / H<sub>2</sub>O<sub>2</sub> y / mmol/L  
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 H<sub>2</sub>O<sub>2</sub>  
 ( L  
 $2\text{H}_2\text{O}_2 \rightarrow 2\text{H}_2\text{O} + \text{O}_2$  ( )  
 $\text{H}_2\text{O}_2 + \text{OH}^0 \rightarrow \text{H}_2\text{O} + \text{HO}_2^0$  ( )  
 Fe<sup>2+</sup> / H<sub>2</sub>O<sub>2</sub>

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H<sub>2</sub>O<sub>2</sub>:CN  
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## The Study of Fenton Performance in Removal of Cyanide from Aqueous Solution

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Received; 18 July 2011 Accepted; 16 October 2011

### ABSTRACT

**Background and Objectives:** Cyanide is a toxic pollutant existing in the various industrial effluents such as iron and steel, coal mining, non-ferrous metals manufacturing and metal plating. Its presence in water resources and wastewater, as serious hazardous substances leads to undesirable effects on both the environment and human. Thus, its concentration control is essential for human health. The main goal of this study was to evaluate Fenton process efficiency in cyanide removal from aqueous solution.

**Materials and Methods:** This is an experimental study Conducted at Lab scale in a batch system. We investigated effect of different variables including; pH, mole ratio of  $\text{Fe}^{2+}/\text{H}_2\text{O}_2$ , contact time, and initial concentration of cyanide. Data were analyzed using Excel software.

**Results:** We found that cyanide with initial concentrations of 0.4 mM/L was reduced by 92 %. This removal result was related to oxidizing agent of hydroxyl radicals under optimum conditions including; pH = 4, molar ratio  $\text{Fe}^{2+}/\text{H}_2\text{O}_2 = 0.046$  ( $\text{Fe}^{2+} = 0.27$  mM/L) after 60 min reaction time. An increase in reaction time was not improved cyanide removal efficiency. Moreover, the Fenton process efficiency in cyanide removal decreased from 92 to 60 %, by increasing the initial cyanide concentration from 0.4 to 0.6 mM/L.

**Conclusion:** It can be concluded that Fenton oxidation Process can be considered as a suitable alternative for cyanide removal to achieve environmental standards.

**Keywords:** Advanced oxidation, Hydrogen peroxide, Fenton, Wastewater treatment, Cyanide

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